

Modeling LNAPL Depletion at a Former Xylene Processing Facility (Germany)

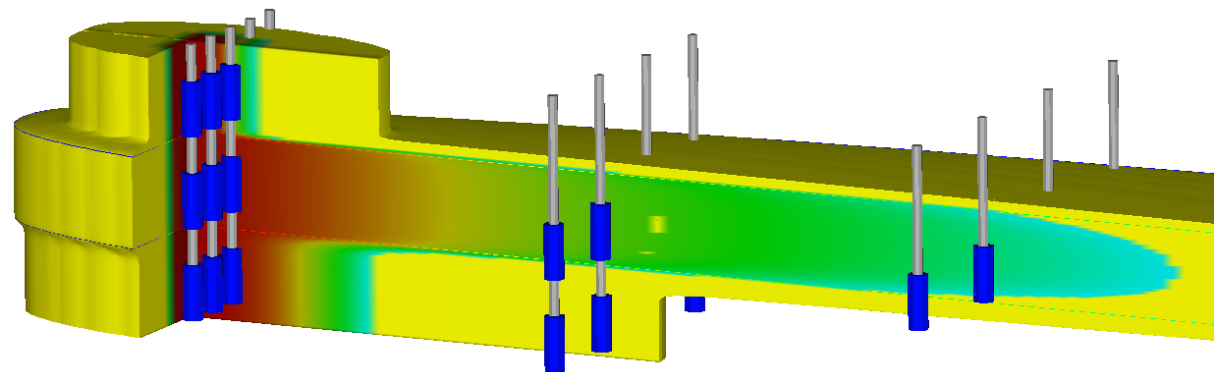
by Grant R. Carey, Ph.D.

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Ottawa, Ontario, Canada

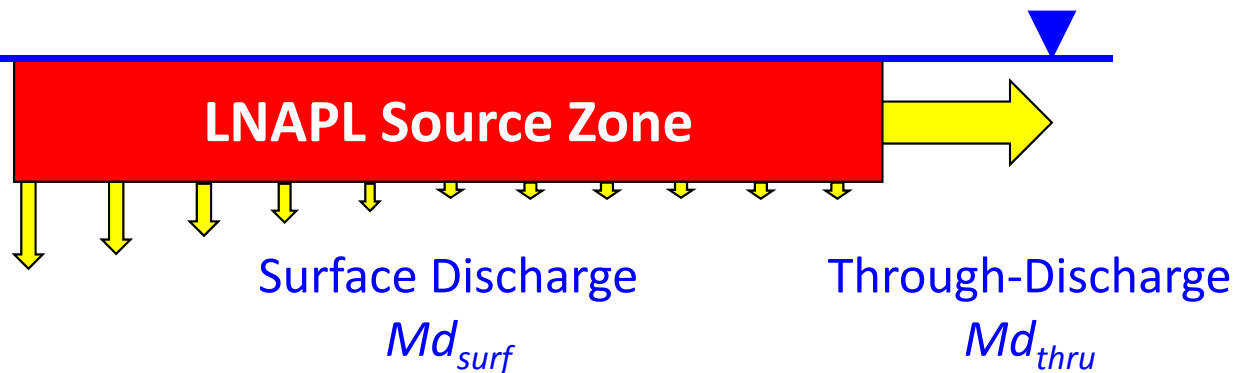
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LNAPL Depletion Modeling

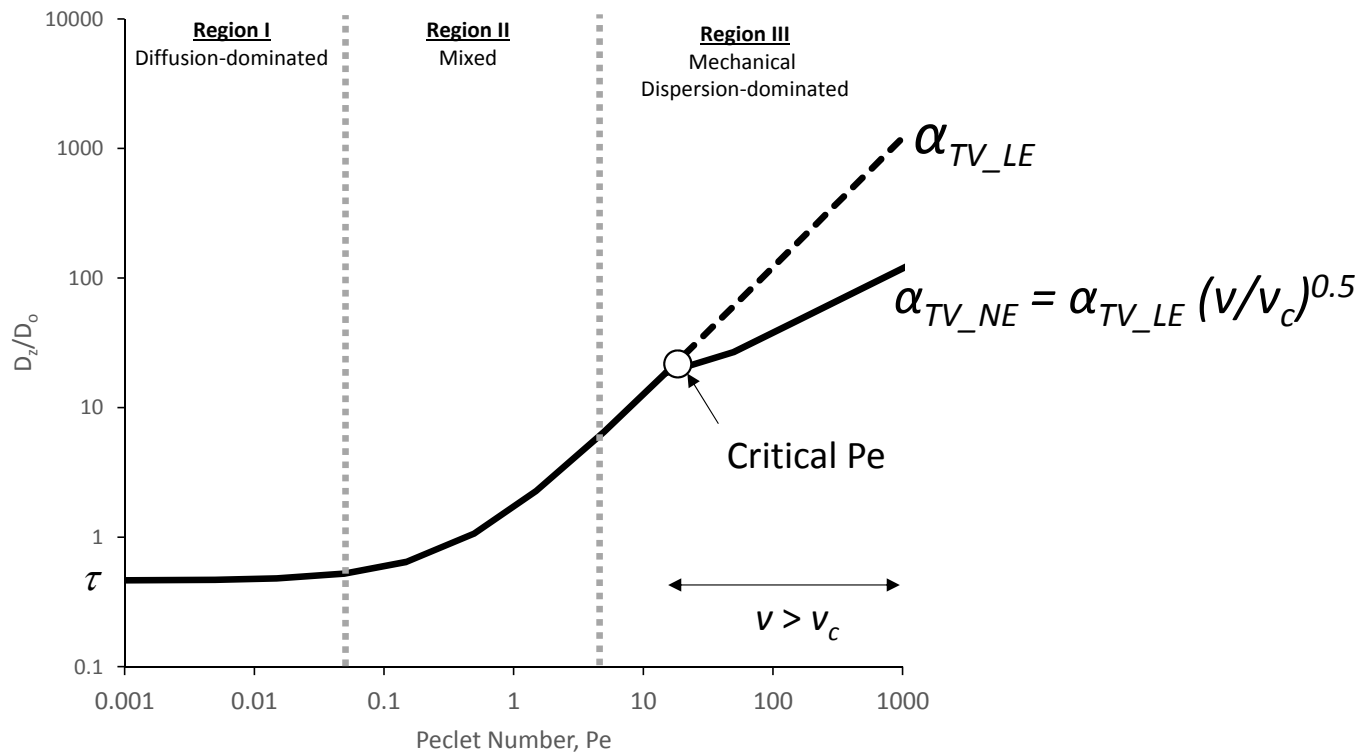


Schafer and Therrien (1995)
Former Xylene Processing Facility

- **Screening Model Uses**
 - Compare Timeframes
 - Refine CSM
 - Identify data gaps
 - Regulatory support
- **Critical field properties**
 - LNAPL thickness
 - Transverse dispersivity
- **Case study example**

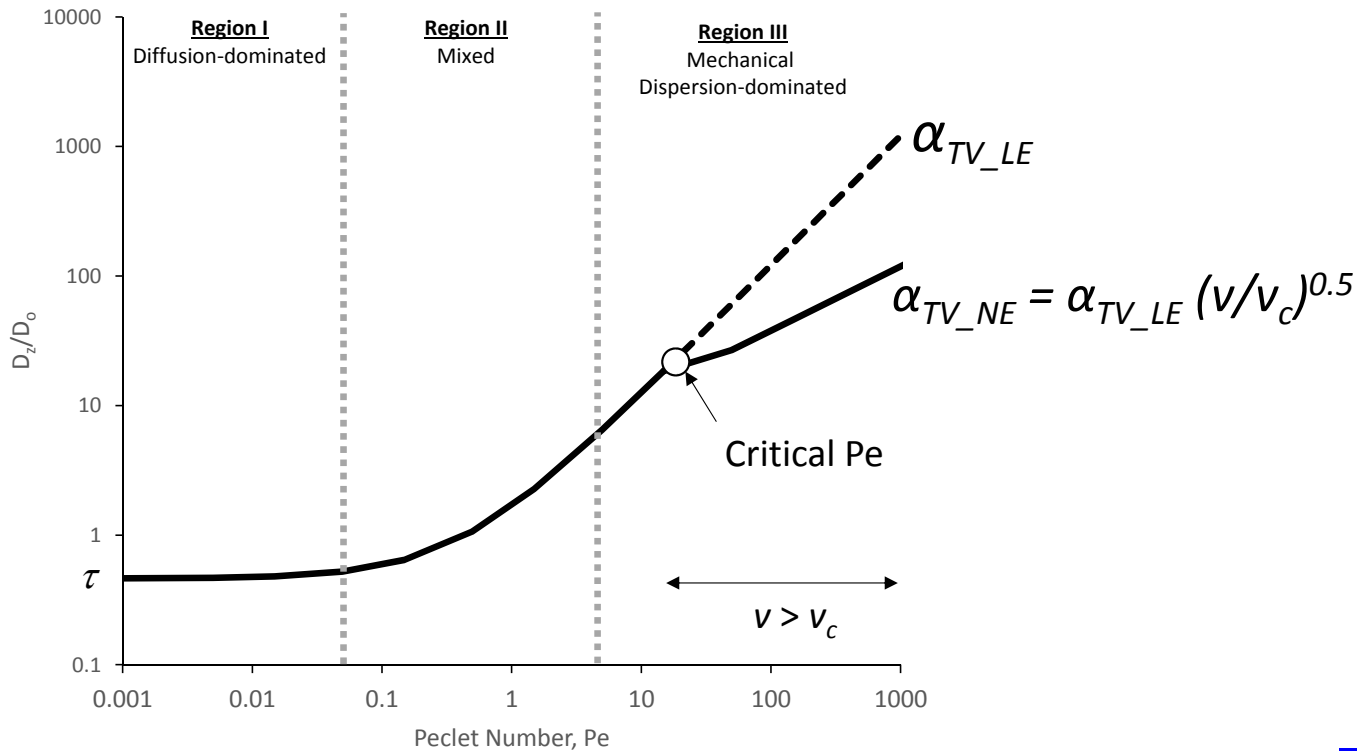
Transverse Vertical Dispersivity

Klenk and Grathwohl (2002), and Carey et al. (2015)

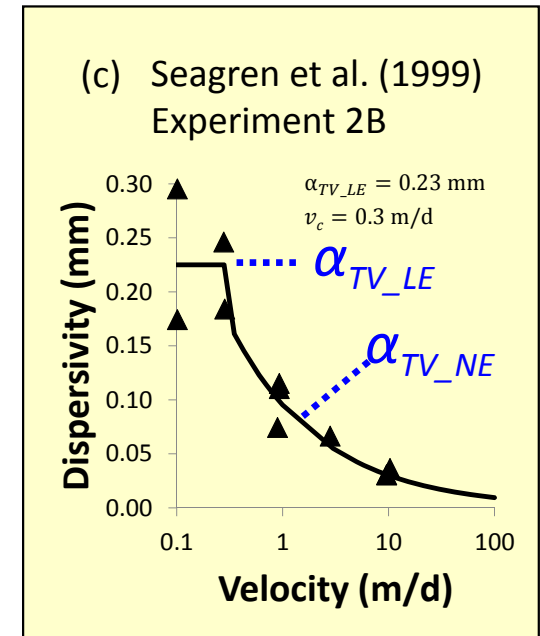


Transverse Vertical Dispersivity

Klenk and Grathwohl (2002), and Carey et al. (2015)



Carey et al. (2015a)



$v_c \sim 3 \text{ to } 5 \text{ m/d}$ for pool dissolution

Transverse Vertical Dispersivity (LE) vs. K

Carey et al. (2015a)

● Lab scale

△ Macro-scale

◇ Olsson and Grathwohl, 2007

× Chiogna et al., 2010

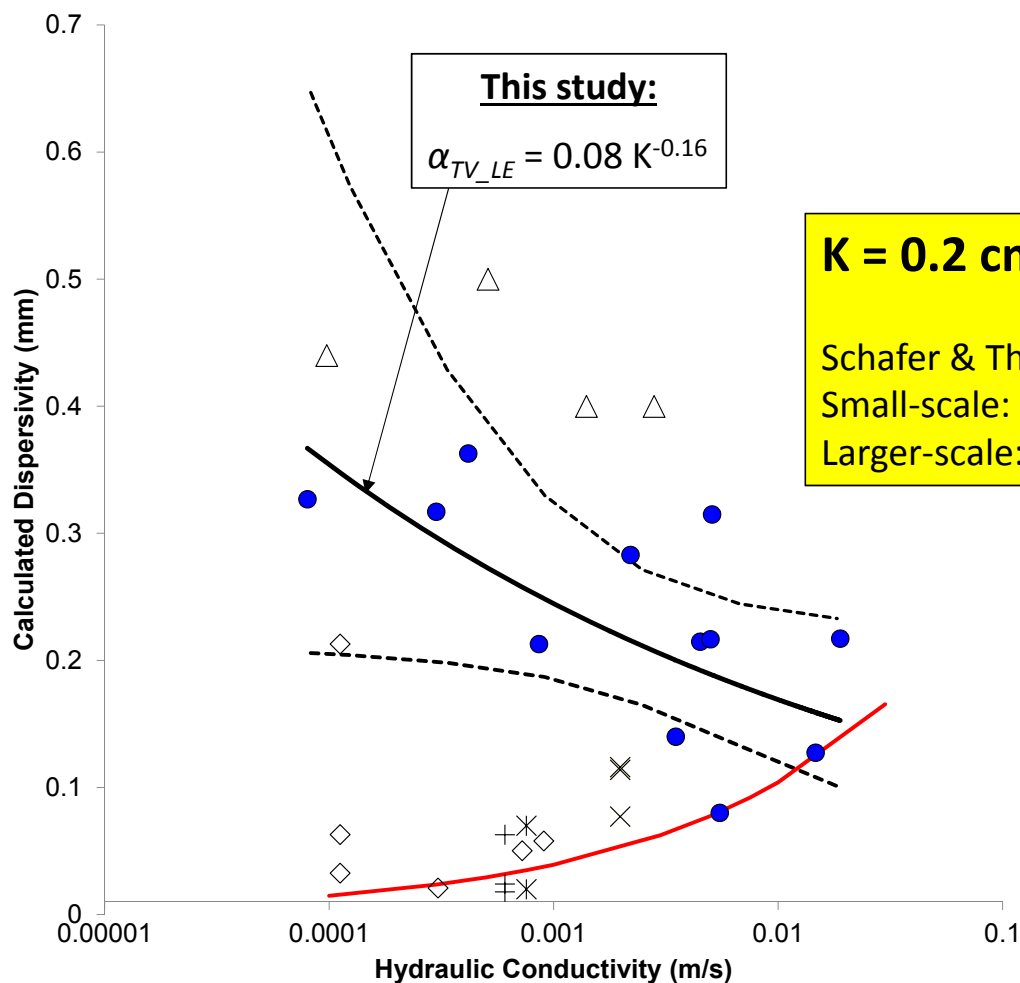
+ Rolle et al, 2012

* Rolle et al, 2013

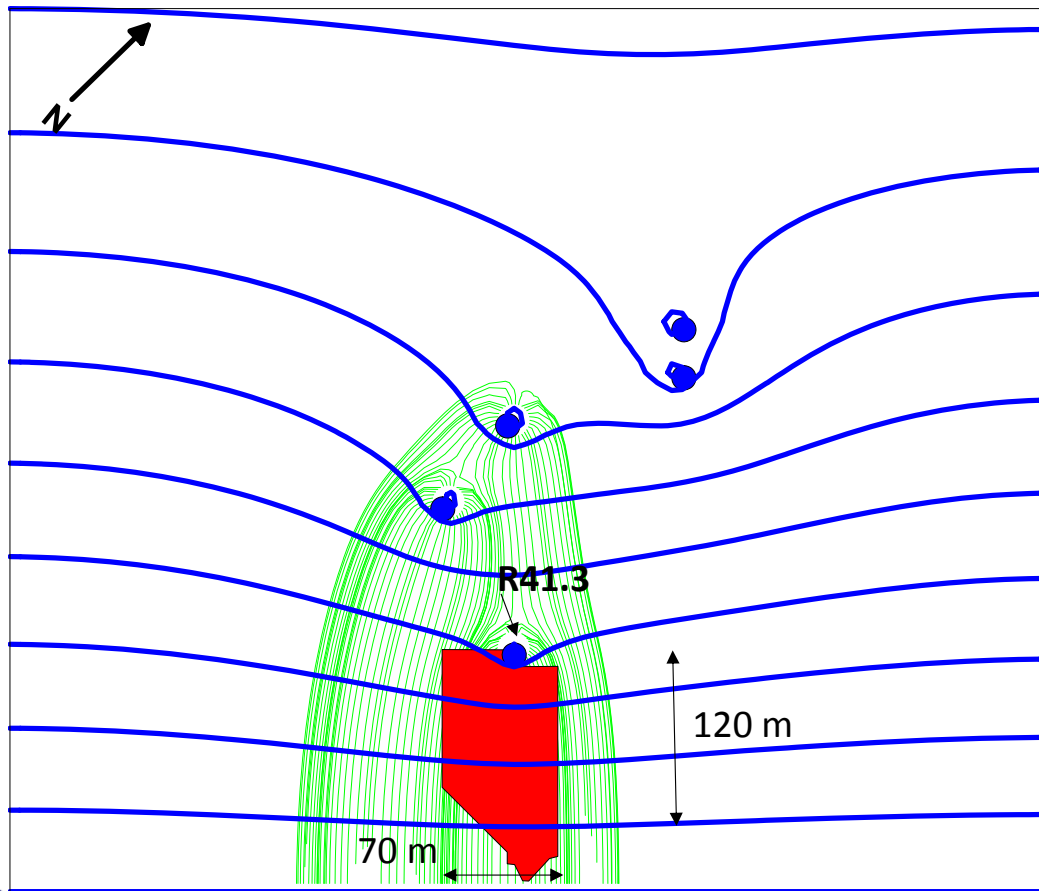
— Regression (this study)

- - - Confidence interval

— Regression (Chiogna et al., 2010)



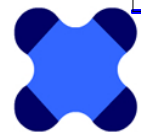
Former Xylene Processing Facility (Germany)



- Groundwater extraction well
- Modeled groundwater elevation contour
- Particle trace
- LNAPL source zone

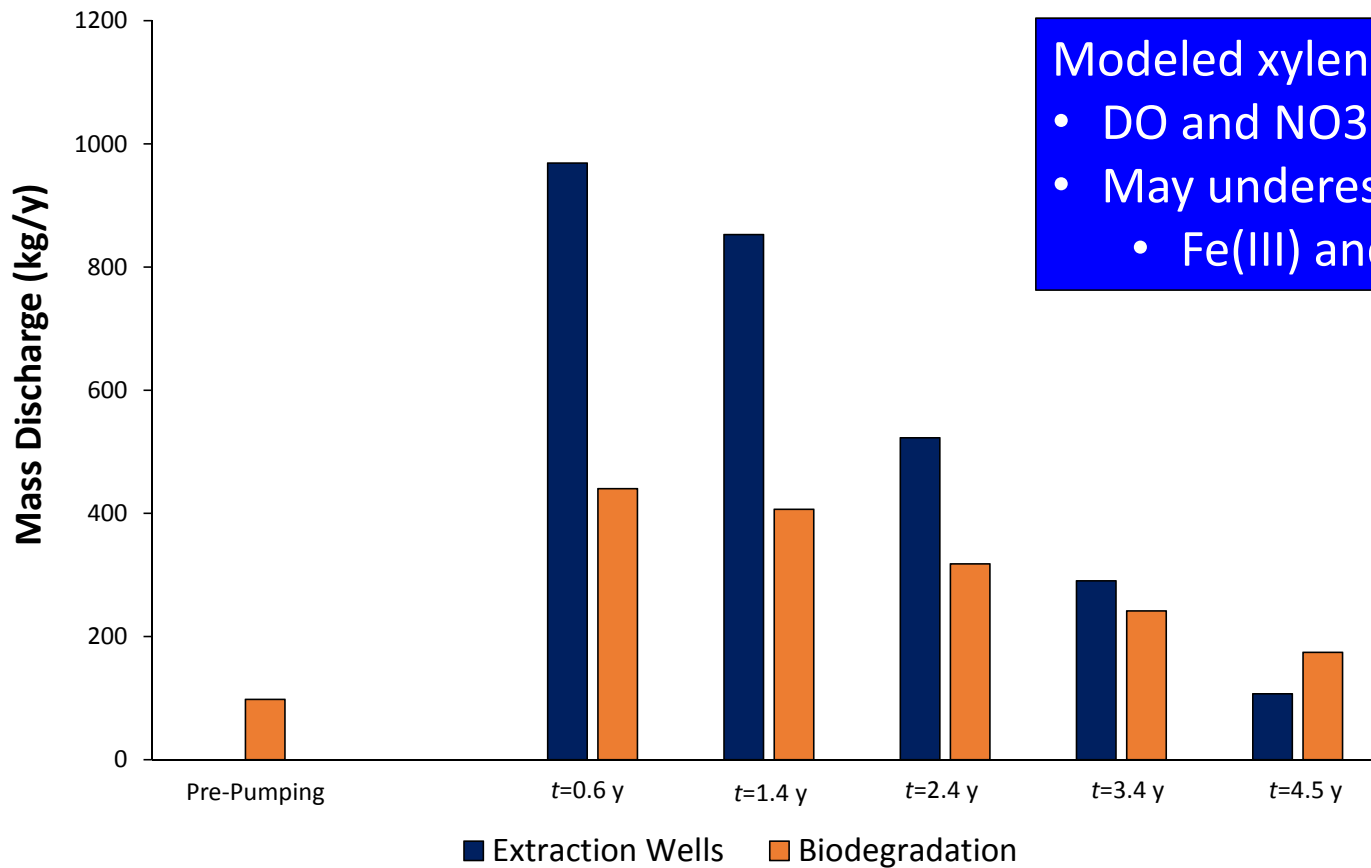
Scale, in meters
0 100 200

Pumping: 4.5 year period



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Estimated Mass Discharge Based on Schafer and Therrien (1995)



Modeled xylene biodegradation

- DO and NO₃ reduction only
- May underestimate actual by 2x
 - Fe(III) and SO₄ reduction

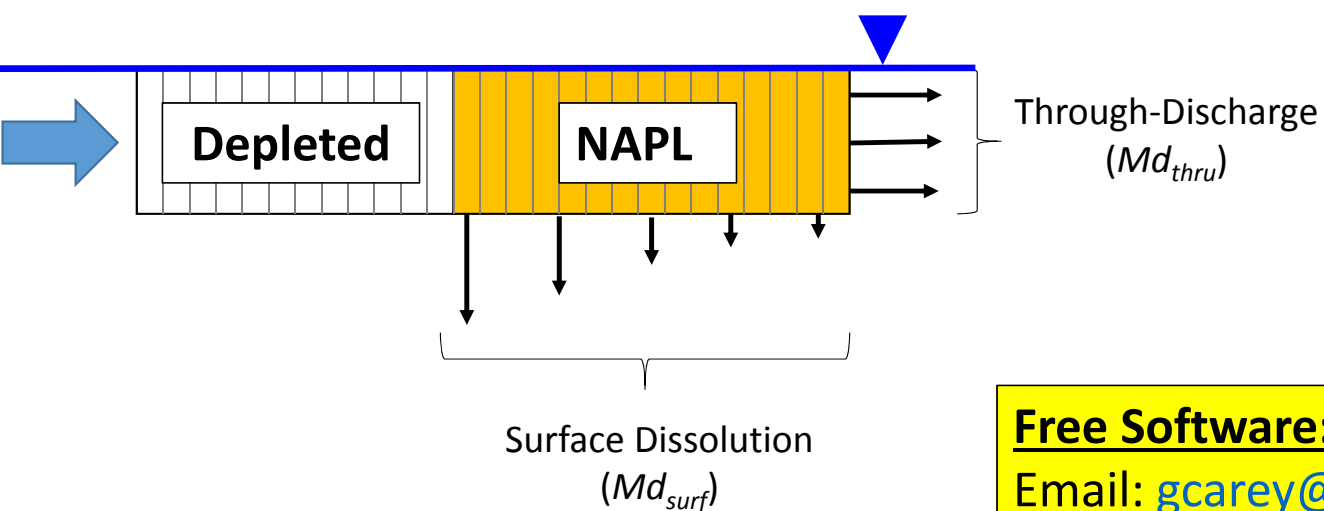


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NAPL Depletion Model (NDM): Mass Discharge

Carey et al. (2014a)



Free Software:

Email: gcarey@porewater.com

Download after Sep. 30th: www.porewater.com

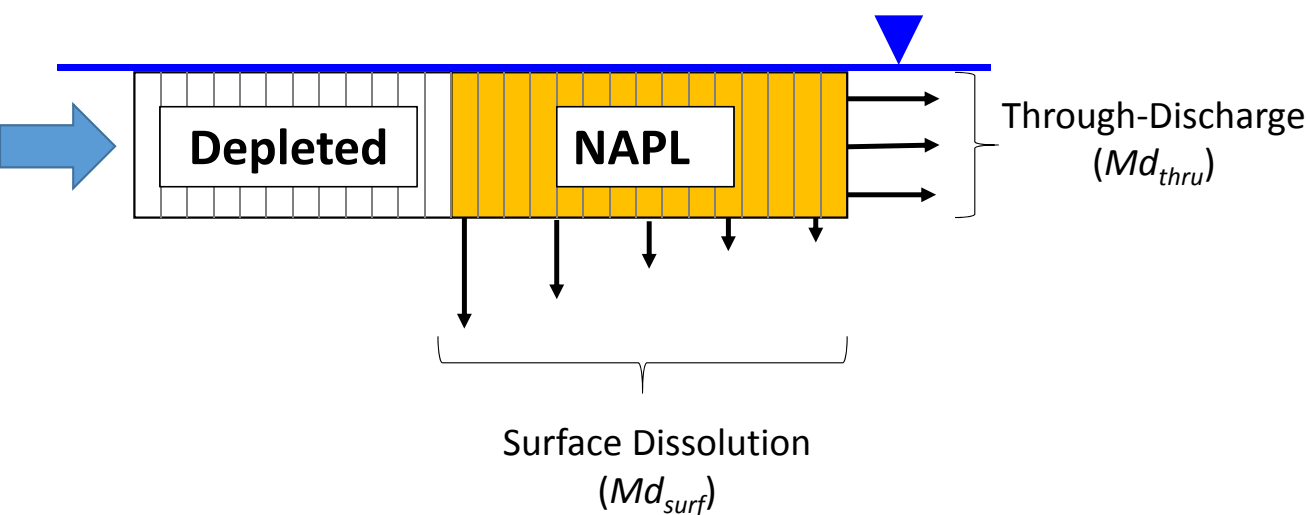


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NAPL Depletion Model (NDM): Mass Discharge

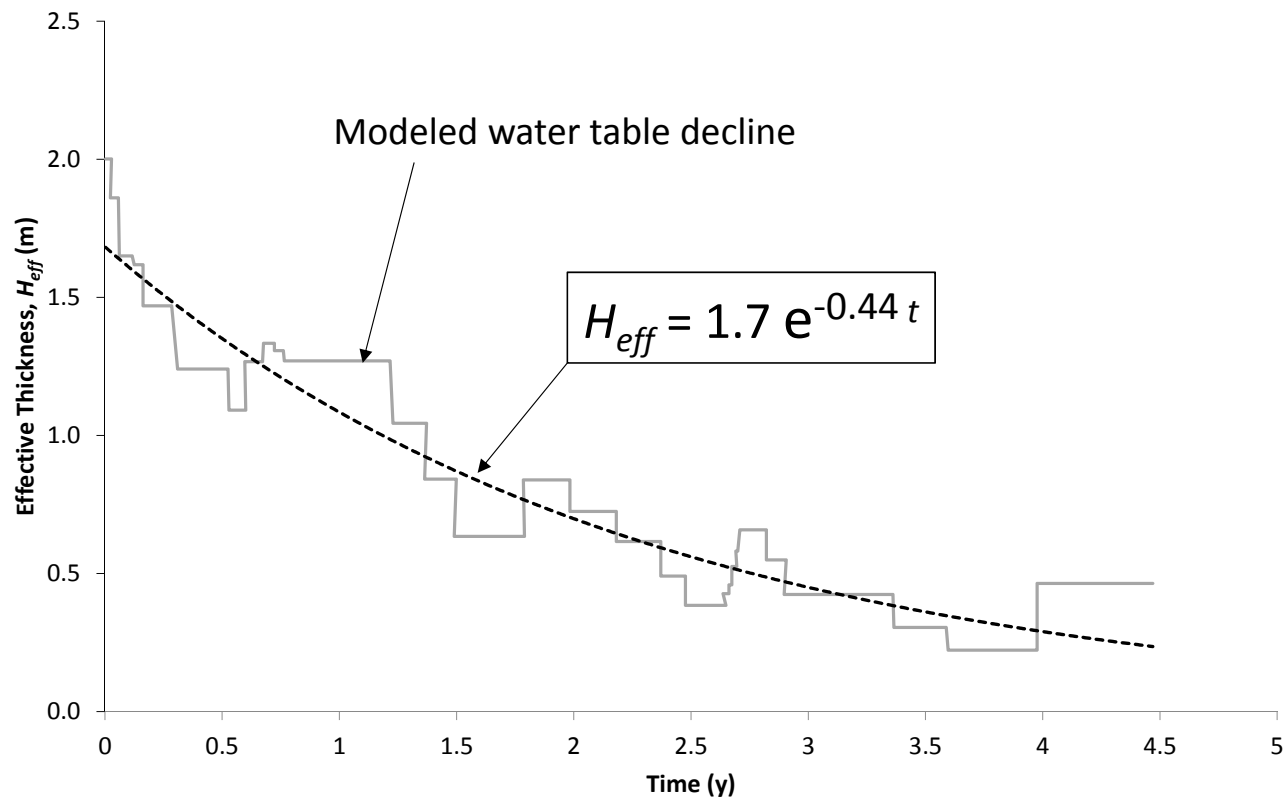
Carey et al. (2014a)



Empirical Relationship (K in m/s)	
$\tau = 0.60 K^{0.030}$	(i)
$\theta_t = 0.30 K^{-0.026}$	(ii)
$\theta_e = 0.41 K^{0.064}, K \leq 1 \times 10^{-2} \text{ m/s}$	(iii)
$\theta_e = (0.29 K^{-0.026}) - 0.03, K > 1 \times 10^{-2} \text{ m/s}$	(iv)
$\alpha_{TV} = 0.08 K^{-0.16}, v \leq v_c$	(v)
$\alpha_{TV_NE} = 0.08 K^{-0.16} (v_c/v)^{0.5}, v > v_c$	(vi)
$\alpha_{aw} = 0.112 (100 K)^{0.211}$	(vii)
$n = 13.14 (100 K)^{0.246} \quad K \geq 1 \times 10^{-4} \text{ m/s}$	(viii)
$S_{wr} = 0.015 (100 K)^{-0.218}$	(ix)

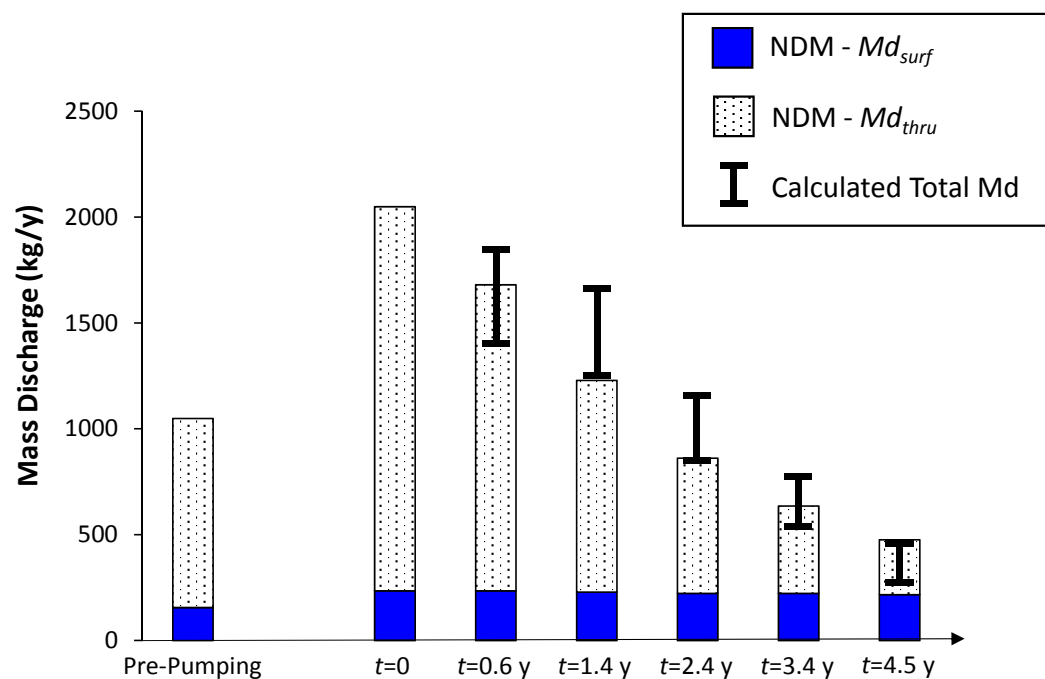
Carey et al. (2015a,b,c)

Saturated Source Zone Thickness vs. Time



Note: Effective thickness of the LNAPL source zone was determined based on an assumed source zone bottom elevation of 19.75 m, and the fluctuating water table elevation. $t=0$ corresponds to May 1, 1988.

Modeled and Estimated Mass Discharge



Notes:

1. Groundwater extraction system started at t=0.
2. Md = mass discharge.
3. Range in calculated total Md is based on the potential difference between including and excluding xylene biodegradation under manganogenesis, ferrogenesis, and sulfate reduction.



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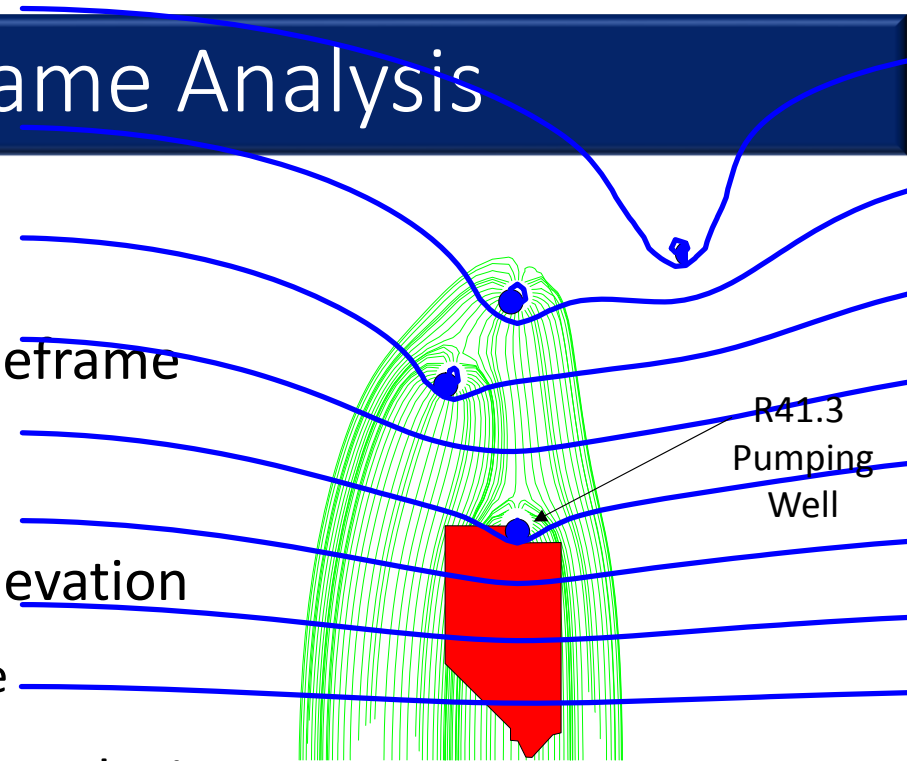
Remediation Timeframe Analysis

Goal

- Evaluate influence of Q on depletion timeframe

Approach

- Assume constant, average water table elevation
 - Source zone 0.85 m thick below water table
- Evaluate influence of increasing Q on GW velocity
- Model LNAPL depletion for each scenario

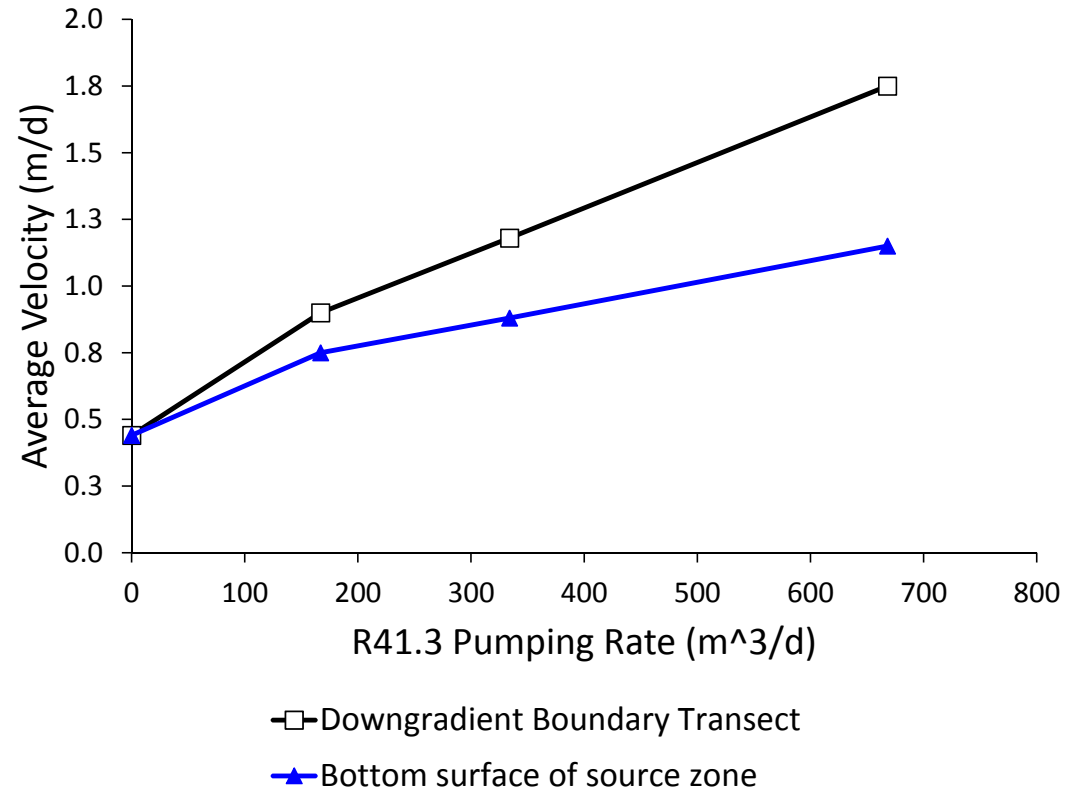
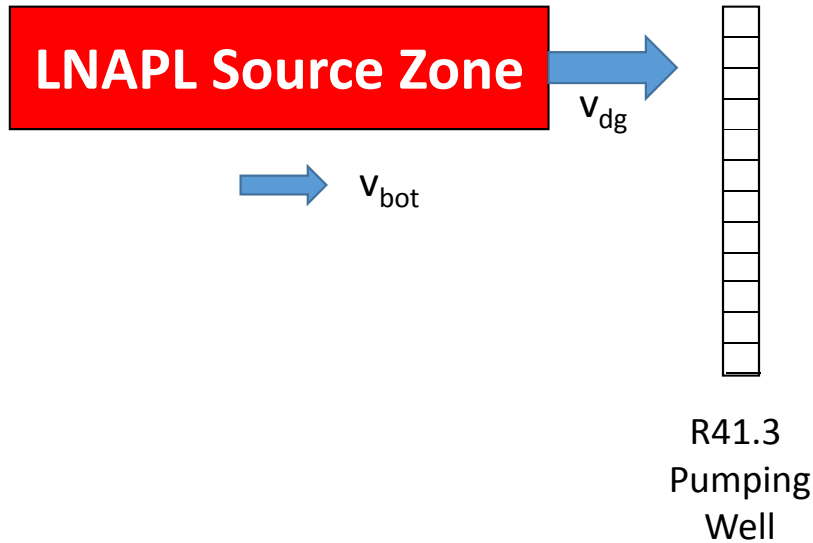


Scenarios

Q=0 (MNA)
Qx1 (system design)
R41.3 Qx2
R41.3 Qx4

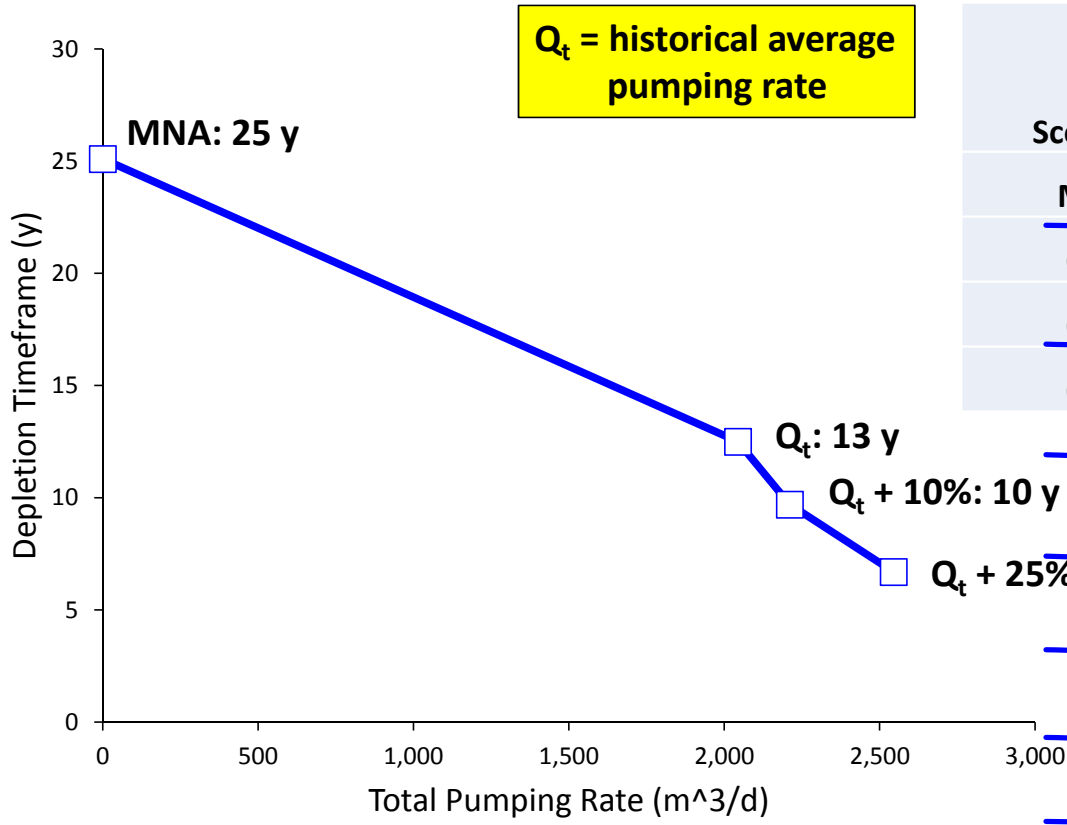


Velocity vs. Pumping Rate

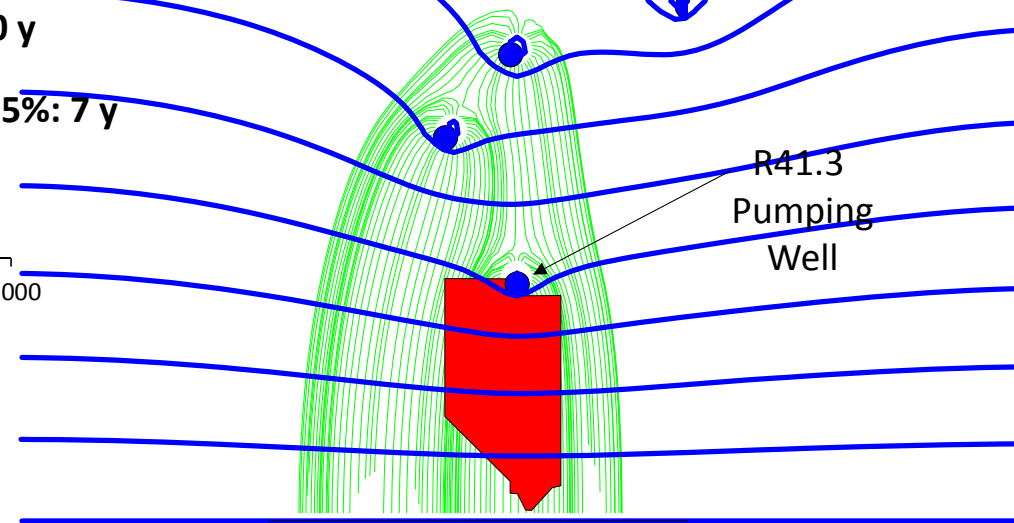


Depletion Timeframe vs. Total Pumping Rate

Q_t = historical average pumping rate



Scenario	R41.3 Pumping Rate (m ³ /d)	Combined Pumping Rate (m ³ /d)	Remediation Timeframe (y)
MNA	0	0	25.1
Qx1	167	2044	12.5
Qx2	334	2211	9.7
Qx4	668	2545	6.7



Summary

- Transverse dispersivity based on K
- Model matched estimated mass discharge vs. time
 - Without any input calibration
- MNA may be appropriate if no receptors at risk
- Increased pumping rate at R41.3
 - Small incremental cost
 - Large reduction in remediation timeframe

Questions



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